

Notes on  
**1.63 Advanced Environmental Fluid Mechanics**  
 Instructor: C. C. Mei, 2001  
 ccmei@mit.edu, 1 617 253 2994

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 2-1-intro.tex

## Chapter 2. Slow viscous flows

Because of the inherent nonlinearity, most problems must be solved by either analytical approximations or by numerical computations. Whenever possible, analytical approximations can be much more effective for gaining physical insight.

In this chapter we shall first explain the lubrication approximation, with applications to the flow of thin layers. Attention will then be turned to the slow flow past a sphere and a cylinder. Application to the environmental problem of aerols will be briefly discussed. Lastly the slow withdrawal of fluid from a stratified reservoir into a sink will be analyzed.

### 2.1 Governing equations for a layer of fluid flowing down an inclined plane

As our first example, we consider the flow of a thin layer of viscous fluid on an inclined plane. Referring to Figure 2.1.1, let the  $x$ -axis coincide with the plane bed inclined at the angle  $\theta$  with respect to the horizon, and the  $y$ -axis normal to the plane bed,

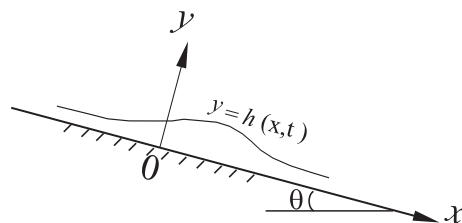


Figure 2.1.1: A thin fluid layer flowing down an incline plane

#### 2.1.1 Exact equations

Continuity :

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2.1.1)$$

Momentum :

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = g \sin \theta - \frac{1}{\rho} \frac{\partial p}{\partial x} + \nu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \quad (2.1.2)$$

and

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -g \cos \theta - \frac{1}{\rho} \frac{\partial p}{\partial y} + \nu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) \quad (2.1.3)$$

## 2.1.2 Boundary conditions

On the rigid bottom no slipping is allowed,

$$u = v = 0, \quad y = 0. \quad (2.1.4)$$

The top of the fluid layer of local depth  $h(x, t)$  is a material surface whose position is unknown until the problem is solved. It is necessary to specify a kinematic boundary condition concerning the motion, and two dynamic conditions concerning the stresses.

### Kinematic condition:

Since the top is a material surface, it must be always composed of the same fluid particles. The fluid velocity must be tangential to the moving surface at all times. Let us describe the top surface by

$$F(\vec{x}, t) = F(x, y, t) \equiv y - h(x, t) = 0 \quad (2.1.5)$$

Consider a surface point which is at  $\vec{x}$  at time  $t$ , then it will move to  $\vec{x} + \vec{q}_s dt$  at time  $t + dt$  where  $dt$  is a very short time interval and  $\vec{q}_s$  is the velocity of the surface point. The new top surface is then described by

$$F(\vec{x} + \vec{q}_s dt, t + dt) = 0$$

Taylor-expanding for small  $dt$ , we get

$$F(\vec{x}, t) + dt \left( \frac{\partial F(\vec{x}, t)}{\partial t} + \vec{q}_s \cdot \nabla F(\vec{x}, t) \right) + O(dt)^2 = 0$$

The first term vanishes because of (2.1.5), hence

$$\frac{\partial F(\vec{x}, t)}{\partial t} + \vec{q}_s \cdot \nabla F(\vec{x}, t) = 0$$

in the limit of  $dt = 0$ . Now the unit normal to the surface is

$$\vec{n} = \frac{\nabla F(\vec{x}, t)}{|\nabla F(\vec{x}, t)|}$$

and the normal component of the surface velocity is  $\vec{q}_s \cdot \vec{n}$ . Since the normal velocity of a fluid particle  $\vec{q}$  on the surface must be equal to the normal velocity of the surface at the same point,

$$\frac{\vec{q}_s \cdot \nabla F(\vec{x}, t)}{|\nabla F(\vec{x}, t)|} = \frac{\vec{q} \cdot \nabla F(\vec{x}, t)}{|\nabla F(\vec{x}, t)|}$$

it follows that

$$\frac{\partial F(\vec{x}, t)}{\partial t} + \vec{q} \cdot \nabla F(\vec{x}, t) = 0 \quad (2.1.6)$$

This is the kinematic boundary condition on the top fluid surface. Substituting  $F = y - h(x, t) = 0$  we get the kinematic boundary condition.

$$\frac{\partial h}{\partial t} + u \frac{\partial h}{\partial x} = v, \quad y = h(x, t) \quad (2.1.7)$$

#### Dynamic boundary conditions

Let the free surface be stress-free:

$$\Sigma_i = (-p\delta_{ij} + \tau_{ij}) n_j = 0, \quad i = 1, 2. \quad (2.1.8)$$

or

$$\Sigma_1 = -pn_1 + \tau_{11}n_1 + \tau_{12}n_2 = 0 \quad (2.1.9)$$

$$\Sigma_2 = -pn_2 + \tau_{21}n_1 + \tau_{22}n_2 = 0. \quad (2.1.10)$$

on  $y = h$ . The unit normal vector has the components:

$$n_1 = -\frac{\frac{\partial h}{\partial x}}{\sqrt{1 + \left(\frac{\partial h}{\partial x}\right)^2}}, \quad n_2 = \frac{1}{\sqrt{1 + \left(\frac{\partial h}{\partial x}\right)^2}} \quad (2.1.11)$$

So far these exact boundary conditions are highly nonlinear, in part because the position for applying these conditions are not known. As an useful consequence of (2.1.7) to be used later, we integrate the continuity equation in depth, to get, after invoking Leibnitz's rule

$$\int_0^h \left( \frac{\partial u}{\partial x} + \frac{\partial v}{\partial z} \right) dz = \frac{\partial}{\partial x} \int_0^h u dx - u(x, h, t) \frac{\partial h}{\partial x} + v(x, h(x, t), t) = 0$$

With the help of (2.1.7), we get the depth-integrated law of mass conservation,

$$\frac{\partial h}{\partial t} + \frac{\partial}{\partial x} \left( \int_0^h u dx \right) = \frac{\partial h}{\partial t} + \frac{\partial Q}{\partial x} = \frac{\partial h}{\partial t} + \frac{\partial(\bar{u}h)}{\partial x} = 0 \quad (2.1.12)$$

where  $Q$  denotes the rate of volume discharge and  $\bar{u}$  the depth averaged horizontal velocity

$$\bar{u} = \frac{Q}{h} = \frac{1}{h} \int_0^h u dy \quad (2.1.13)$$